

# Highly active and stable amorphous IrO<sub>x</sub>/CeO<sub>2</sub> nanowires for acidic oxygen evolution

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## ABSTRACT

Development of highly active and durable electrocatalysts for acidic oxygen evolution reaction (OER) remains an unresolved grand challenge. Here, we reported the amorphous IrO<sub>x</sub>/CeO<sub>2</sub> nanowires as highly active and acid-stable OER catalysts through a facile electro-spinning/calcination approach. The amorphous catalysts delivered a high mass activity of 167 A g<sub>Ir</sub><sup>-1</sup> at 1.51 V, a low overpotential of 220 mV at 10 mA cm<sup>-2</sup>, and a stable performance for 300 h of continuous operation in acid. As revealed by complementary experimental and theoretical calculation results, the intimate nanoscale feature of IrO<sub>x</sub>/CeO<sub>2</sub> creates abundant binary interfaces, at which CeO<sub>2</sub> as an electron buffer regulates the adsorption of oxygen intermediates, lowers the activation barrier of OER, and suppresses the over-oxidation and dissolution of Ir, thereby significantly enhancing the OER activity and stability. This work provides a new strategy for designing highly active and acid-resistant OER catalysts.

## 1. Introduction

The development of renewable energy relies heavily on energy conversion and storage technologies to mitigate the intermittency problems associated with wind and solar power. In addition to lithium-sulfur batteries, sodium-ion batteries, and metal-air batteries [1–4], electrocatalytic water oxidation, especially the oxygen evolution reaction (OER), plays a pivotal role in renewable energy production and storage technologies [5]. However, the state-of-the-art OER electrocatalysts are significantly limited by their relatively low efficiency and seriously unsatisfactory stability, which are predominantly ascribed to the catalytically sluggish OER kinetics and dynamically alternated physicochemical properties of the catalyst surfaces during operations, such as the alternated chemical compositions, (electro) chemical etching, aggregation, surface reconstruction, phase change, etc. [6–8]. Especially, the longevity of most OER electrocatalysts in acidic conditions is a grand challenge owing to the highly oxidizing and corrosively

acidic operating environments. At the same time, the proton exchange membrane water electrolyzers exhibit many benefits for overall water splitting and show more promise for practical applications compared to the counterpart of alkaline electrolyzers [9–11]. Thus, developing efficient and stable water oxidation electrocatalysts in acidic media is challenging yet highly expected.

Many efforts have been placed on rationalizing acidic OER electrocatalysts with high activity and stability. To date, IrO<sub>x</sub>, RuO<sub>x</sub>, and their derivatives show the best OER catalytic performance in acidic media, in which Ir-based oxides show better stability but less activity than Ru-based oxides [12–14]. Extensive studies have been conducted to improve the acidic OER activity of Ir-based electrocatalysts by exposing more active sites and modulating the local electronic structures [15–20]. Despite those advances, both the life-time and activity of IrO<sub>x</sub> as well as their derivatives, are still far from the expectation for practical applications. Although the deactivation mechanisms are still incomplete and under intense debate, the activity deterioration of Ir-based OER

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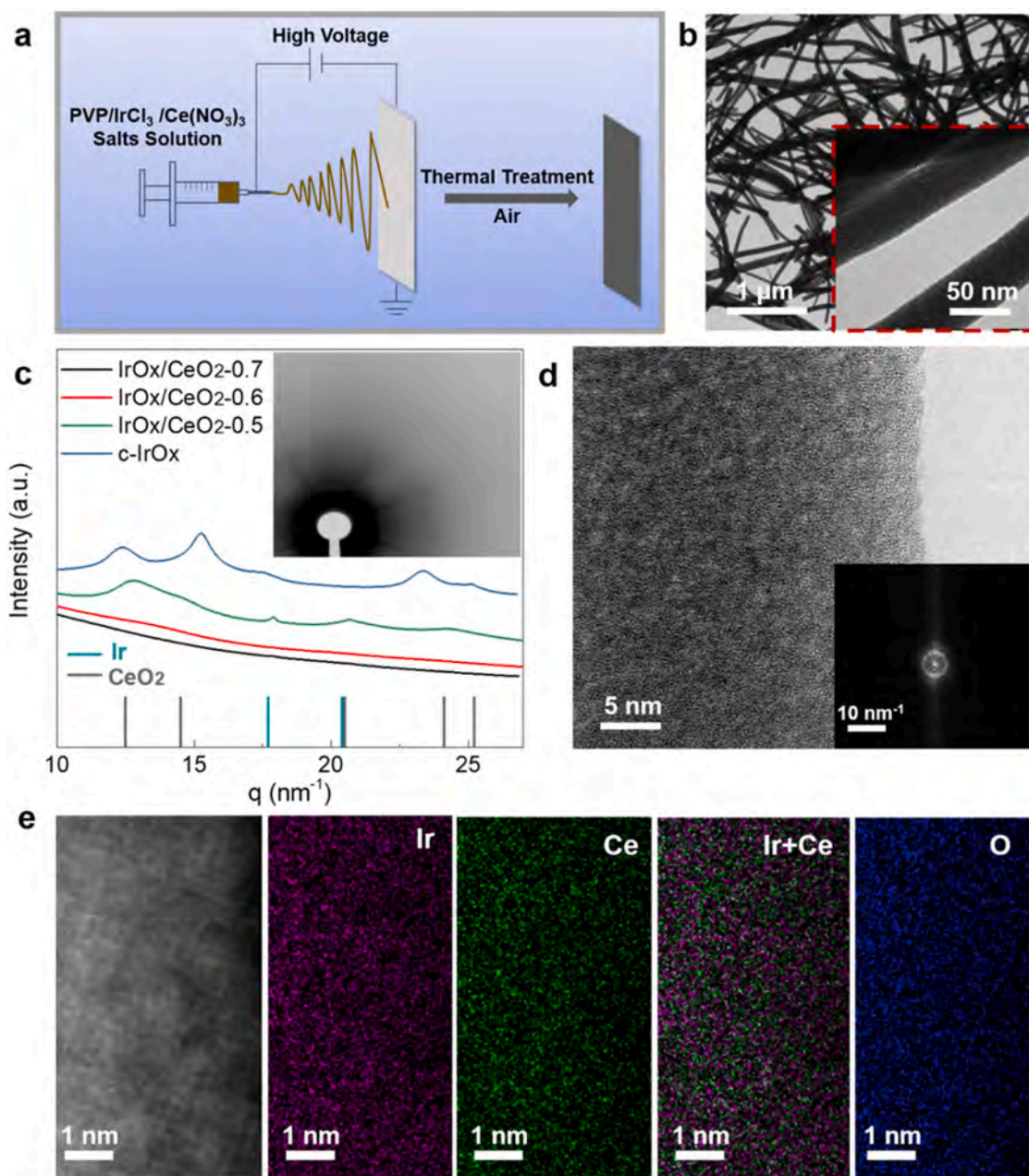
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electrocatalysts can be generally attributed to the dissolution of iridium under the applied potentials in acidic electrolytes. The detailed deactivation mechanism investigations suggested that the formation of unstable Ir species induced the dominant Ir-dissolution under dynamic operating conditions, which were determined by the initial phases and structures of Ir-based electrocatalysts [21,22]. Among them, the amorphous  $\text{IrO}_x$  electrocatalysts exhibited improved activity due to the facile formation of reactive electrophilic  $\text{O}^{\text{I-}}$  oxygen species on the amorphous surface with the mixed-oxidation state of  $\text{Ir}^{3+/4+}$  [23,24]. However, except for the in-situ electrooxidation of Ir metals, the facile methods for synthesizing amorphous iridium oxide are scarce. Moreover, continuous and gradual deactivation is still inevitable due to the transient reduction and oxidation between  $\text{Ir}^{4+}$  and  $\text{Ir}^{3+}$  as the predominant dissolution pathway for amorphous  $\text{IrO}_x$  electrocatalysts. Also, the formation of unstable  $\text{Ir}^{>4+}$  leads to poor stability for amorphous  $\text{IrO}_x$  electrocatalysts

and crystalline  $\text{IrO}_2$  [25]. Even though the reasons for the dissolution of iridium-based catalysts are controversial, the consensus has been reached that aggressive change of oxidation states of interfacial iridium species leads to the dissolution of electrocatalysts. Inspired by these recognitions, integrating an electron buffer with  $\text{IrO}_x$  could be a feasible strategy to stabilize the oxidation states of iridium, which could theoretically minimize and even completely suppress the dissolution of iridium under the highly anodic and/or corrosive acidic OER environment.

$\text{CeO}_2$  with the reversible  $\text{Ce}^{3+}/\text{Ce}^{4+}$  redox pair has been widely introduced as an electronic promoter to modulate the local electronic structures of host electrocatalysts (e.g.,  $\text{IrO}_x$ ,  $\text{Co}_3\text{O}_4$ , metal phosphides, layered double hydroxide) and thereby enhance their performance for OER [26–29]. Most of those hybrid electrocatalysts for OER were performed in basic environments rather than in acidic electrolytes.



**Fig. 1.** Synthesis and characterizations. (a) Illustration of the synthetic procedure. (b) TEM images of  $\text{IrO}_x/\text{CeO}_2$ -0.6 nanowires. Inset shows the nanowire morphology with high-resolution and detail. (c) SAXS spectra of  $\text{IrO}_x/\text{CeO}_2$ - $y$  and  $c\text{-IrO}_x$ . Inset shows the image plate of  $\text{IrO}_x/\text{CeO}_2$ -0.6. (d) HRTEM image of  $\text{IrO}_x/\text{CeO}_2$ -0.6. Inset shows the corresponding fast Fourier transform pattern. (e) The HAADF-STEM image and corresponding elemental maps of  $\text{IrO}_x/\text{CeO}_2$ -0.6.

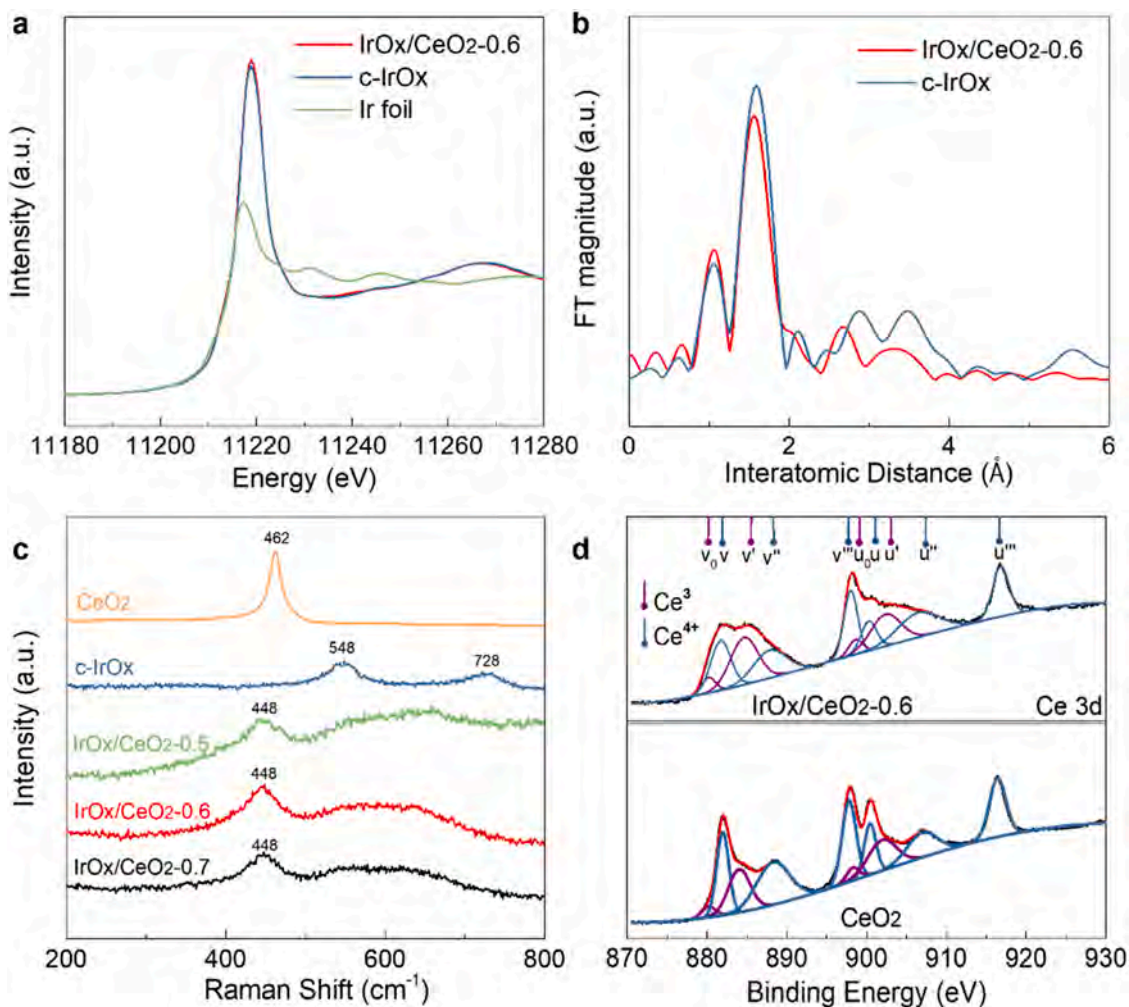
Nevertheless, the integration of CeO<sub>2</sub> and IrO<sub>x</sub> has not yet been explored for acidic OER. Motivated by those advances of CeO<sub>2</sub>-incorporated electrocatalysts for basic OER and the high chemical stability of CeO<sub>2</sub> in acidic media, integrating CeO<sub>2</sub> and IrO<sub>x</sub> and understanding CeO<sub>2</sub> as the electronic modulators on the local electronic structures of iridium species can provide a new approach to improve catalytic activity and stability of IrO<sub>x</sub> for acidic OER.

Herein, using a facile electro-spinning synthesis methodology, we present highly active and stable amorphous IrO<sub>x</sub>/CeO<sub>2</sub> nanowire electrocatalysts for water oxidation in 0.5 M H<sub>2</sub>SO<sub>4</sub>. The catalysts are featured by nanoscale intimacy and amorphous structure of the binary subnanometer-scale mixed IrO<sub>x</sub> and CeO<sub>2</sub> particles in the nanowires, thereby providing abundant interfaces and favorable kinetics for acidic OER. In comparison with the commercially available IrO<sub>x</sub> (c-IrO<sub>x</sub>), the catalysts deliver a significantly high activity (220 mV of overpotential at 10 mA cm<sup>-2</sup> and 167 A g<sub>Ir</sub><sup>-1</sup> of mass activity) and a highly stable OER performance (> 300 h) in acid. Catalytic mechanism investigations illustrate that CeO<sub>2</sub> as an electron buffer not only enhances the catalytic activity of amorphous IrO<sub>x</sub> but also lowers the Ir oxidation states during OER, thereby suppressing the iridium dissolution and ultimately exhibiting a highly active and robust performance for acidic OER.

## 2. Results and discussion

### 2.1. Synthesis and characterizations of amorphous IrO<sub>x</sub>/CeO<sub>2</sub> nanowire

Amorphous IrO<sub>x</sub>/CeO<sub>2</sub> nanowire electrocatalysts were prepared through a facile electro-spinning method from a sol precursor containing IrCl<sub>3</sub> and Ce(NO<sub>3</sub>)<sub>3</sub> and sequential thermal treatments at high temperatures (Fig. 1a, see Experimental section in Supporting Information for details). The chemical compositions of the electrocatalysts were modulated by the initial molecular ratios of metal precursors. The electrocatalysts were named as IrO<sub>x</sub>/CeO<sub>2</sub>-y, where y represented the molar percentage of iridium. Initially, the morphology of electrocatalysts was examined by transmission electron microscopic (TEM, Fig. 1b and Fig. S1). The uniform wire-like morphology of the electrocatalysts with a diameter of ~50 nm and a length of several microns was observed as the molar ratios of Ir/Ce were larger than 1.0. When the molar proportion of Ce increased by over 50 %, the uniform nanowire morphology could not be maintained, accompanied by the irregular micron particles (Fig. S2). Structural features of the electrocatalysts were also characterized by small-angle X-ray scattering (SAXS, Fig. 1c) [30]. Comparing to the pronounced diffraction patterns of the commercial rutile c-IrO<sub>x</sub> catalysts, no obvious diffraction peaks of IrO<sub>x</sub>/CeO<sub>2</sub>-0.7 and IrO<sub>x</sub>/CeO<sub>2</sub>-0.6 indicated the amorphous feature (Fig. S3), which was further confirmed by high-resolution TEM (HRTEM) images (Fig. 1d) and the selected area electron diffraction (SAED) patterns (inset of Fig. 1d) [31]. Meanwhile, the faint reflections of IrO<sub>x</sub>/CeO<sub>2</sub>-0.5 suggest a mixed phase of metallic



**Fig. 2.** X-ray adsorption and Raman spectra. (a) Iridium L-edge XANES spectra for IrO<sub>x</sub>/CeO<sub>2</sub>-0.6 and c-IrO<sub>x</sub>. (b) EXAFS spectra for IrO<sub>x</sub>/CeO<sub>2</sub>-0.6 and c-IrO<sub>x</sub>. (c) Raman spectra for IrO<sub>x</sub>/CeO<sub>2</sub>, c-IrO<sub>x</sub> and CeO<sub>2</sub>. (d) XPS spectra of Ce 3d for IrO<sub>x</sub>/CeO<sub>2</sub>-0.6 and CeO<sub>2</sub>.

Ir and fluorite CeO<sub>2</sub>. Through the control experiments, the suitable amount of cerium oxide (Fig. S4) and the appropriate calcination temperature (Fig. S5) guaranteed the formation of the amorphous structure. Energy-dispersive X-ray spectroscopy (EDS) elemental maps indicated the uniform distribution of iridium, cerium, and oxygen of IrO<sub>x</sub>/CeO<sub>2</sub>-0.6 at the nanoscale (Fig. 1e). The EDS result (Fig. S6) further confirmed that the actual ratio of Ir and Ce of IrO<sub>x</sub>/CeO<sub>2</sub>-0.6 was 5.6:4.4, being close to the nominal ratios in the precursor mixtures.

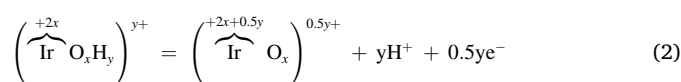
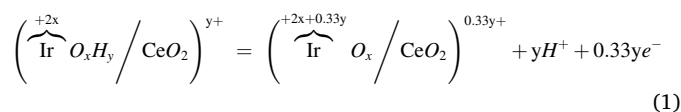
## 2.2. Oxidation states of amorphous IrO<sub>x</sub>/CeO<sub>2</sub> nanowires

The electronic and local geometrical structures of IrO<sub>x</sub>/CeO<sub>2</sub>-0.6 were characterized by X-ray absorption fine structure spectroscopy (XAFS), where the Ir foil and c-IrO<sub>x</sub> catalysts were used as references. As shown in their X-ray absorption near edge structure (XANES) spectra (Fig. 2a), the Ir L<sub>III</sub> edge spectra of IrO<sub>x</sub>/CeO<sub>2</sub>-0.6 displayed a similar spectral shape and edge position to that of c-IrO<sub>x</sub>, indicating their nearly identical electronic structure in the bulk phase. Moreover, the extended X-ray absorption fine structure (EXAFS) spectra of IrO<sub>x</sub>/CeO<sub>2</sub>-0.6 and c-IrO<sub>x</sub> showed the Ir-O contribution at a distance of 1.98 Å in the [IrO<sub>6</sub>] octahedron (Fig. 2b), demonstrating the nearly identical Ir-O local geometrical structure between IrO<sub>x</sub>/CeO<sub>2</sub>-0.6 and c-IrO<sub>x</sub>. The iridium coordination number of 5.3 of IrO<sub>x</sub>/CeO<sub>2</sub>-0.6 was slightly lower than that of bulk c-IrO<sub>x</sub> (5.7), suggesting the smaller size of IrO<sub>x</sub> in amorphous nanowires [31,32]. Raman spectroscopy was then conducted to explore the vibration of surface species on the electrocatalysts (Fig. 2c). Comparing to the Raman shift of Ce-O F<sub>2g</sub> vibration of the reference CeO<sub>2</sub> sample synthesized by the same electrospun method at 462 cm<sup>-1</sup>, three IrO<sub>x</sub>/CeO<sub>2</sub>-y catalysts exhibited the significantly broadened and red shifted vibration peaks of Ce-O F<sub>2g</sub> at 448 cm<sup>-1</sup>. It could be attributed to the fact that the amorphous structure is generally more disordered and has longer average cerium-oxygen bonds than the crystalline phase. This finding demonstrates the Ce-O coordination on the surface of amorphous catalysts showing a similar local structure to CeO<sub>2</sub> [33, 34]. The c-IrO<sub>x</sub> catalysts displayed the characterized Raman shifts of Ir-O vibrations at ~548 and 728 cm<sup>-1</sup>. The broad Raman peaks of IrO<sub>x</sub>/CeO<sub>2</sub>-y from 510 cm<sup>-1</sup> to 740 cm<sup>-1</sup> were attributed to the two broadened peaks of Ir-O as well as one vibration peak of surface oxygen vacancies in CeO<sub>2</sub> (600 cm<sup>-1</sup>) [35]. Taking all characterizations together, we can deduce that Ir and Ce species in the catalysts show a similar local structure with IrO<sub>2</sub> and CeO<sub>2</sub>, respectively. Considering the uniform elemental distribution in Fig. 1, the bulk catalysts can be regarded as a uniform combination of IrO<sub>2</sub> and CeO<sub>2</sub> with nanoscale intimacy. The significant lattice mismatch between IrO<sub>2</sub> and CeO<sub>2</sub> grains results in an extremely-low-crystallinity state. Overall, the amorphous IrO<sub>x</sub>/CeO<sub>2</sub> nanowires herein show the structural features of the nanoscale intimacy of binary components of IrO<sub>x</sub> and CeO<sub>2</sub> with the spatial proximity, providing abundant interfaces of IrO<sub>x</sub>/CeO<sub>2</sub> in electrocatalysts.

The oxidation states of Ir and Ce at the surface of the IrO<sub>x</sub>/CeO<sub>2</sub>-0.6 were analyzed by X-ray photoelectron spectroscopy (XPS). XPS spectra of Ir 4f (Fig. S7) suggest a similar mixture of Ir<sup>4+</sup> and Ir<sup>3+</sup> on the surfaces of both IrO<sub>x</sub>/CeO<sub>2</sub>-0.6 and c-IrO<sub>x</sub> [36]. The surface trivalent and tetravalent cerium were monitored by deconvolution of Ce 3d core-level XPS spectra (Fig. 2d). The Ce 3d and O 1s (Fig. S8) spectra indicate a higher surface fraction of Ce<sup>3+</sup> (37.4 %) associated with abundant oxygen vacancies on the surface of IrO<sub>x</sub>/CeO<sub>2</sub>-0.6, compared with the as-synthesized CeO<sub>2</sub> (Ce<sup>3+</sup>% = 24.3%) through the similar method [37, 38]. Electron energy loss spectrum (EELS) also shows a mixture of Ce<sup>3+</sup>/Ce<sup>4+</sup> with a high-intensity ratio of M<sub>5</sub>/M<sub>4</sub> peaks (Fig. S9), consistent with the XPS analysis [39,40]. Determined from ultraviolet photoelectron spectroscopy (UPS, Fig. S10), the position of the valence-band edge of the IrO<sub>x</sub>/CeO<sub>2</sub>-0.6 catalyst was about zero and near to E<sub>f</sub>. Therefore, the IrO<sub>x</sub>/CeO<sub>2</sub>-0.6 catalysts showed the nearly same conducting properties as that of the commercial iridium oxide [41].

## 2.3. CeO<sub>2</sub> as an electron buffer

To experimentally explore the fundamental role of CeO<sub>2</sub>, operando cyclic voltammetry (CV) was conducted to monitor the redox behavior of various catalysts. Throughout the continuous CV scanning, the position and currents of the redox peaks become stabilized. As shown in Fig. S11, the redox pair at 1.27 V (anodic) and 1.33 V (cathodic) was assigned to the deprotonation and re-protonation of the catalyst surface. The deprotonation/re-protonation process also affects Ir's oxidation states [42]. After that, we conducted a pH-dependence analysis of the cathodic peak on the IrO<sub>x</sub>/CeO<sub>2</sub>-0.6 and c-IrO<sub>x</sub> catalysts in 0.5 M H<sub>2</sub>SO<sub>4</sub> solution in the pH range of 0.36–1.26 (Fig. 3a and Fig. S12). The peak potentials vs. standard hydrogen electrode were plotted against the solution pH values. The slope of 198.3 ± 12.8 mV per pH unit of IrO<sub>x</sub>/CeO<sub>2</sub>-0.6 suggests a 1e<sup>-</sup>/3 H<sup>+</sup> coupled redox process, which is different from the 120 ± 3.0 mV per pH unit of c-IrO<sub>x</sub> with a 1e<sup>-</sup>/2 H<sup>+</sup> process (Fig. 3b) [43,44]. The pre-oxidation process can be described by the following equations:

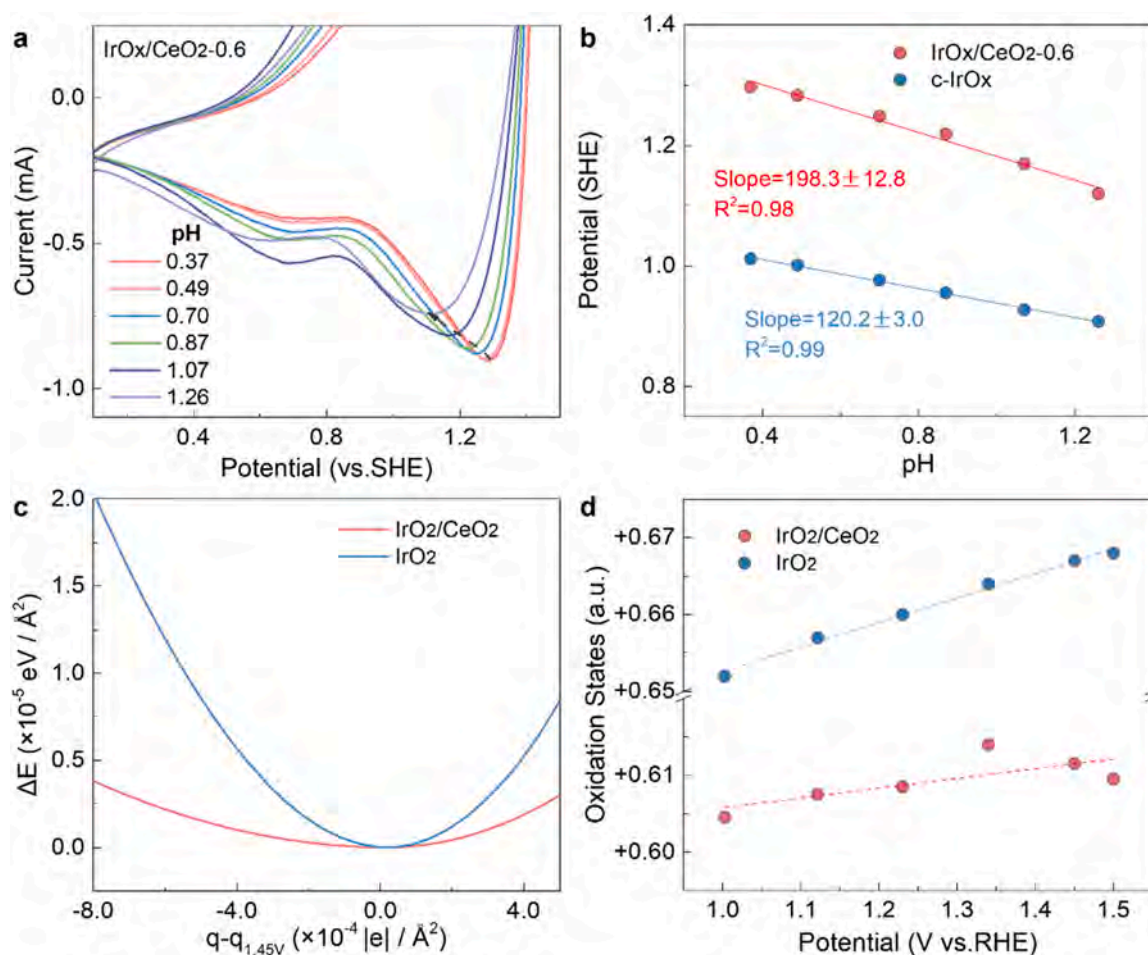


The averaged oxidation states are labeled at the top of Ir. Ir species in IrO<sub>x</sub>/CeO<sub>2</sub> show a smaller increase of oxidation states compared to the IrO<sub>x</sub> alone. Thus, we can make preliminary speculation that CeO<sub>2</sub> can act as an electron buffer to inhibit the over-oxidation of interfacial Ir species. In addition, CV curves of IrO<sub>x</sub>/CeO<sub>2</sub>-0.6 and c-IrO<sub>x</sub> recorded at different scan rates in 0.5 M H<sub>2</sub>SO<sub>4</sub> solution (Fig. S13) reveal the first-order power law relationship between the cathodic peak current densities and the scan rate (Fig. S14), suggesting that they are associated with a surface capacitive process [45].

Density functional theory (DFT) calculations were also conducted to examine the capability of CeO<sub>2</sub> as an electron buffer. The IrO<sub>2</sub>/CeO<sub>2</sub> heterojunction model cannot be built by assembling of IrO<sub>2</sub> slab and CeO<sub>2</sub> slab because of their large lattice mismatch. To solve this problem, a Ce<sub>3</sub>O<sub>6</sub>-cluster was constructed on the IrO<sub>2</sub> (110) slab, followed by an ab initio molecular dynamics (AIMD) process. The detailed modeling methodology can be found in Fig. S15. The electronic capacitance properties were studied using a fix-potential method by JDFTx [46]. Assuming a quasi-equilibrium state in U<sub>0</sub> = 1.45 V vs. RHE, an equilibrium quantity of charge (q<sub>1.45 v</sub>) on the electrode will be spontaneously maintained to achieve an energy minimum of the system. Any charge disturbance (q-q<sub>1.45 v</sub>) of the electrode will lead to an energy increment, as shown in Fig. 3c. IrO<sub>2</sub>/CeO<sub>2</sub> can hold or release electrons only at the cost of a smaller energy increment compared to pure IrO<sub>2</sub>. With the assistance of CeO<sub>2</sub>, the oxidation state of the surface Ir sites is stably maintained in a wide potential range (Fig. 3d). Therefore, CeO<sub>2</sub> is an electron buffer that stabilizes the oxidation state of Ir sites.

## 2.4. CeO<sub>2</sub> as an electron buffer for activity

To experimentally explore the fundamental catalytic properties of amorphous nanowires in the acidic electrolyte, we carried out a series of electrochemical measurements in 0.5 M H<sub>2</sub>SO<sub>4</sub> solution by a three-electrode configuration with a graphite rod as the counter electrode and Ag/AgCl as the reference electrode. The catalyst loading for all electroactive materials was controlled at the total weight loading of 0.56 mg cm<sup>-2</sup>. Initially, the electrocatalytic activity was evaluated by linear sweep voltammetry (LSV) method (Fig. 4a). The LSV curves of both IrO<sub>x</sub>/CeO<sub>2</sub>-0.6 and IrO<sub>x</sub>/CeO<sub>2</sub>-0.7 exhibited a sharp increased anodic current response starting at almost the same onset potential

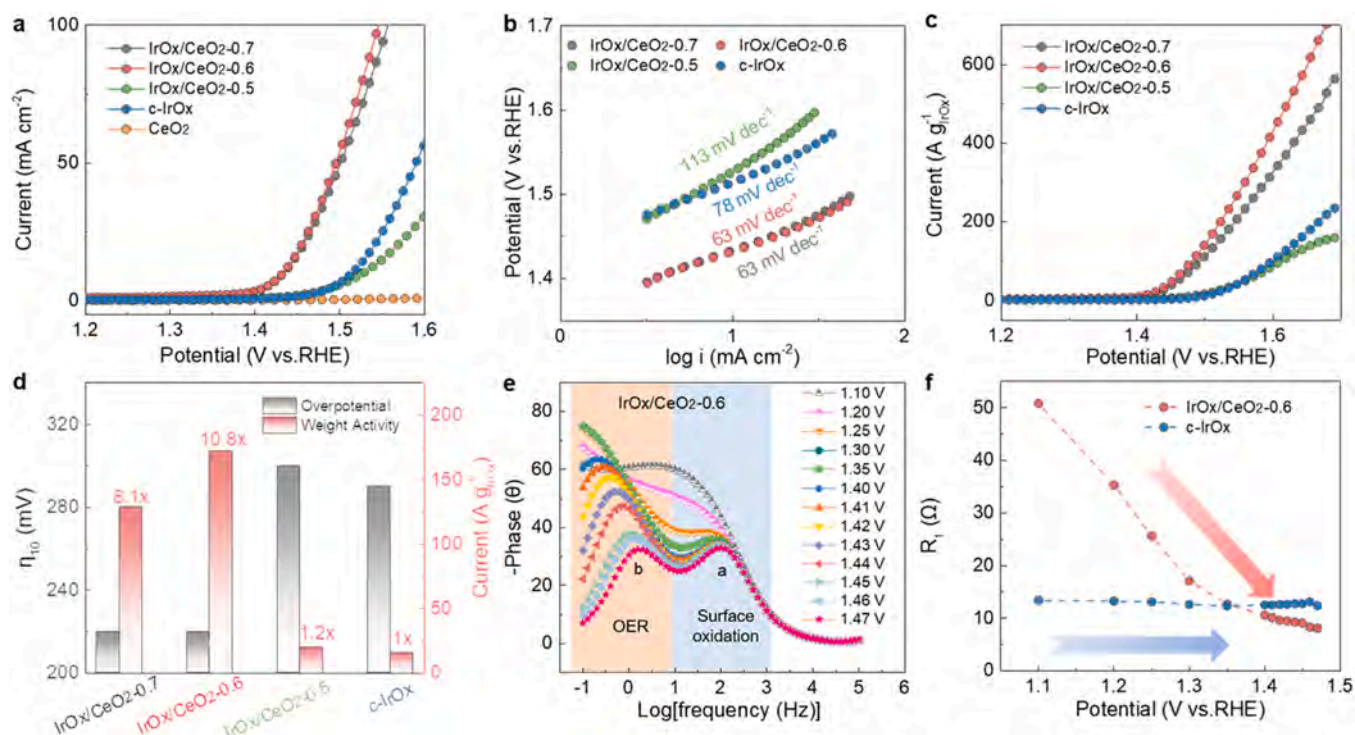


**Fig. 3.** The pH-dependence and oxidation state analysis of the catalysts. (a) CV curves of IrO<sub>x</sub>/CeO<sub>2</sub>-0.6 recorded in H<sub>2</sub>SO<sub>4</sub> solutions with different pH values. (b) The plots of the cathodic peak potential vs. SHE plotted against the solution pH for IrO<sub>x</sub>/CeO<sub>2</sub>-0.6 and c-IrO<sub>x</sub>. (c) The energy cost for the electrode to hold or release extra charges. (d) The averaged oxidation states of surface Ir in different potentials, which were calculated according to the Lowdin population by the built-in algorithm in JDFTx.

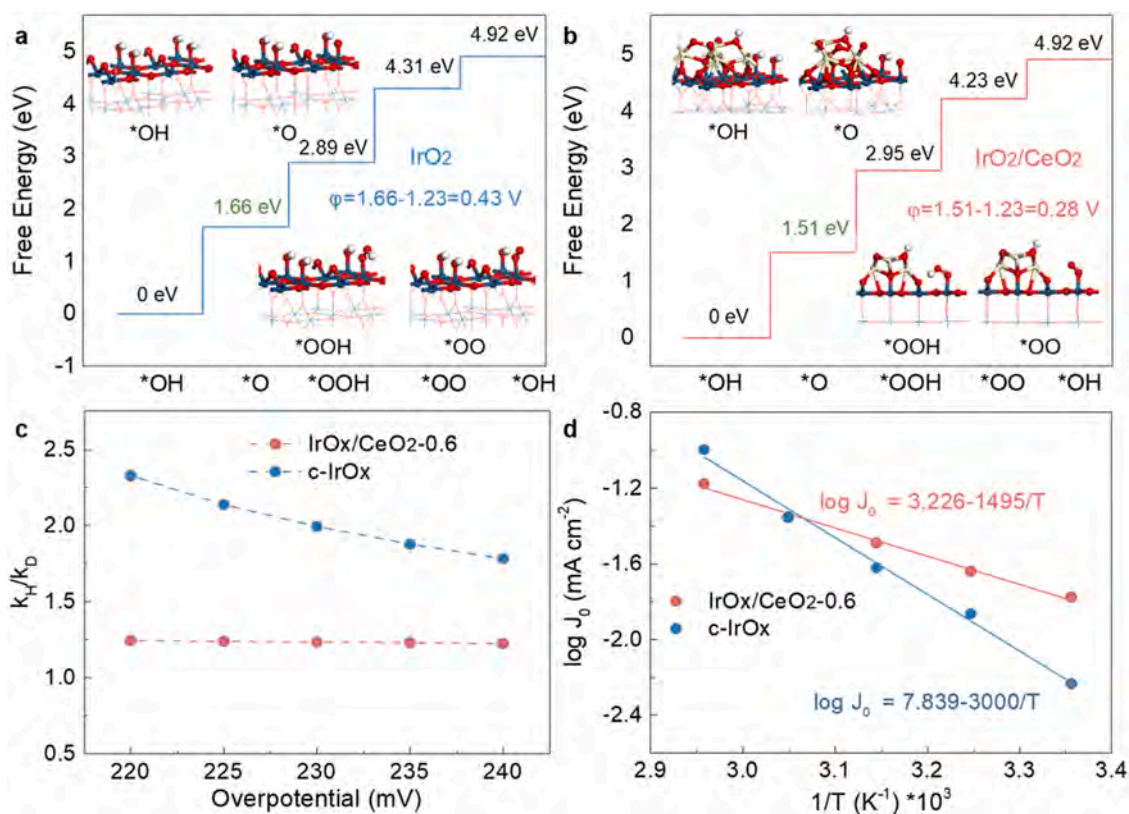
( $E_{\text{onset}}$ , the potential required to reach a specific current density of  $0.1 \text{ mA cm}^{-2}$ ) of 1.37 V, indicating a greatly improved catalytic activity in comparison with other electrodes ( $E_{\text{onset}}=1.45 \text{ V}$  for IrO<sub>x</sub>/CeO<sub>2</sub>-0.5,  $E_{\text{onset}}=1.46 \text{ V}$  for c-IrO<sub>x</sub> and  $E_{\text{onset}}=1.65 \text{ V}$  for CeO<sub>2</sub>). Due to the high Ir-loading in IrO<sub>x</sub>/CeO<sub>2</sub>-0.7 and slightly better catalytic performance of IrO<sub>x</sub>/CeO<sub>2</sub>-0.6, among various catalysts, IrO<sub>x</sub>/CeO<sub>2</sub>-0.6 was recognized as the best electrocatalysts to deliver the highest activity in the window of the applied potentials. The overpotential of IrO<sub>x</sub>/CeO<sub>2</sub>-0.6 for reaching  $10 \text{ mA cm}^{-2}$  ( $\eta_{10}$ ) was 220 mV, which was much lower than those of IrO<sub>x</sub>/CeO<sub>2</sub>-0.5 (300 mV) and c-IrO<sub>x</sub> (290 mV). The use of LSV curves to determine Tafel slope and exchange current density ( $J_0$ ) provides insights into the catalytic kinetics of a given electrocatalyst, where the small Tafel slope and large  $J_0$  generally suggest fast reaction kinetics. Notably, the IrO<sub>x</sub>/CeO<sub>2</sub>-0.6 catalysts exhibited the smallest Tafel slope of  $63 \text{ mV dec}^{-1}$  and the largest  $J_0$  of  $16.8 \text{ } \mu\text{A cm}^{-2}$  at room temperature, compared with those of IrO<sub>x</sub>/CeO<sub>2</sub>-0.5 (Tafel slope =  $113 \text{ mV dec}^{-1}$  and  $J_0 = 12.6 \text{ } \mu\text{A cm}^{-2}$ ) and c-IrO<sub>x</sub> (Tafel slope =  $78 \text{ mV dec}^{-1}$  and  $J_0 = 5.8 \text{ } \mu\text{A cm}^{-2}$ ). This observation suggests the significantly accelerated reaction kinetics in the rate-determined step and the higher electrocatalytic activity of amorphous IrO<sub>x</sub>/CeO<sub>2</sub>-0.6 nanowires for OER under the operating conditions (Fig. 4b). Also, IrO<sub>x</sub>/CeO<sub>2</sub>-0.6 gave out the highest Ir-mass activity of  $167 \text{ A g}_{\text{IrOx}}^{-1}$  at 1.51 V, which was 10.8 times higher than that of c-IrO<sub>x</sub> under the same external potential (Fig. 4c and d). The electrochemical active area of each catalyst was measured by cyclic voltammetry (Fig. S16) and the intrinsic activity of each catalyst was also evaluated (Fig. S17). IrO<sub>x</sub>/CeO<sub>2</sub>-0.6 catalyst showed the

highest intrinsic activity. The measured Faradaic efficiency of O<sub>2</sub> production from the IrO<sub>x</sub>/CeO<sub>2</sub>-0.6 catalyst was 97.4 %.

Interfacial charge transfer between electrocatalysts and adsorbates is the essential step for electrocatalytic reactions. Operando electrochemical impedance spectroscopy (EIS), an effective method to identify charge transfer on the catalyst interface, was employed to analyze the structure-activity relationship and catalytic kinetics between the evolution of electrode surface species and OER. Fig. 4e and Fig. S18 illustrate the Bode plots of the measured impedance of the OER process on IrO<sub>x</sub>/CeO<sub>2</sub>-0.6 and c-IrO<sub>x</sub> in 0.5 M H<sub>2</sub>SO<sub>4</sub> solution from 1.10 V to 1.48 V. The corresponding Bode phase plots were fitted with an equivalent circuit (Fig. S20). The phase Peak a described by  $R_1$  and  $CPE_1$  in the high-frequency region ( $10^1$ - $10^3 \text{ Hz}$ ) is caused by the surface-oxidation interface [47]. Unlike the barely changed  $R_1$  of c-IrO<sub>x</sub>, the resistance of  $R_1$  of IrO<sub>x</sub>/CeO<sub>2</sub>-0.6 became smaller along with the increasing applied potentials, representing a potential-dependent electron transfer in the presence of CeO<sub>2</sub> (Fig. 4f). Beyond an applied potential of 1.35 V, the resistance of  $R_1$  of IrO<sub>x</sub>/CeO<sub>2</sub>-0.6 became smaller than that of c-IrO<sub>x</sub>, which could be attributed to the faster kinetics and more involved electrons on the surface-oxidation interface [48].  $R_2$  and  $CPE_2$  between the frequency region  $10^1$ - $10^1 \text{ Hz}$  represent the adsorption behavior of intermediates on the catalyst surface during the OER process. The  $R_2$  of IrO<sub>x</sub>/CeO<sub>2</sub>-0.6 was lower than that of c-IrO<sub>x</sub> beyond 1.40 V, demonstrating much faster kinetics in adsorbed intermediates during OER (Fig. S21a). The accumulation of reaction intermediates of IrO<sub>x</sub>/CeO<sub>2</sub>-0.6 derived from more than two times larger  $CPE_2$  during the



**Fig. 4.** Electrochemical OER performance. (a) LSV curves of various catalysts at a scanning rate of  $10 \text{ mV s}^{-1}$  in  $0.5 \text{ M H}_2\text{SO}_4$ . (b) Tafel plots for  $\text{IrO}_x/\text{CeO}_2-0.6$  and  $\text{c-IrO}_x$ . (c) LSV curves of various catalysts normalized by unit mass of iridium oxide. (d) Comparison of overpotentials at a current density of  $10 \text{ mA cm}^{-2}$  and the normalized current densities based on a mass of iridium oxide at  $1.51 \text{ V}$  versus RHE. (e) Bode phase plots of  $\text{IrO}_x/\text{CeO}_2-0.6$ . (f) Response of the  $R_1$  charge transfer resistance to the applied potential of  $\text{IrO}_x/\text{CeO}_2-0.6$  and  $\text{c-IrO}_x$ .



**Fig. 5.** DFT calculations, kinetic isotope effect (KIE), and activation energy analyses. (a) The free energy diagram and reaction pathways for OER on  $\text{IrO}_2$ . (b) The free energy diagram and reaction pathways for OER on  $\text{IrO}_2/\text{CeO}_2$ . (c) The calculated  $k_H/k_D$  values under different overpotentials. (d) Arrhenius plot of  $\text{IrO}_x/\text{CeO}_2-0.6$  and  $\text{c-IrO}_x$ .

OER process could benefit the overall catalytic driving force (Fig. S21b) [49]. Overall, the charge-transfer resistance ( $R_{ct}=R_1+R_2$ ) of  $\text{IrO}_x/\text{CeO}_2-0.6$  was smaller than that of  $\text{c-IrO}_x$ , indicating that  $\text{CeO}_2$  as the electron buffer facilitated electron transfer and intermediates adsorption and thus enhanced the intrinsic catalytic activity of  $\text{IrO}_x$  [50].

Theoretically, Ir sites in the simulated model covered with  $^*\text{OH}$  have the lowest formation energy, and thus  $^*\text{OH}$  is the intermediate with the highest coverage during the reaction (Fig. S22 and S23).  $^*\text{OH}$  is the TOF-determining initial state (TDI) according to the energetic span model and thereby we consider  $^*\text{OH}$  as the first intermediate of the reaction cycle [51]. The generation of every oxygen molecule requires four electrons, which can be divided into four electrochemical steps. 1)  $^*\text{OH} \rightarrow ^*\text{O} + \text{H}^+ + \text{e}^-$ ; 2)  $^*\text{O} + \text{H}_2\text{O} \rightarrow ^*\text{OOH} + \text{H}^+ + \text{e}^-$ ; 3)  $^*\text{OOH} \rightarrow ^*\text{OO} + \text{H}^+ + \text{e}^-$ ; 4)  $^*\text{OO} + \text{H}_2\text{O} \rightarrow ^*\text{OH} + \text{O}_2 + \text{H}^+ + \text{e}^-$ . The Gibbs free energy change of each step and the energy diagrams are shown in Fig. 5a and b. On both  $\text{IrO}_2$  and  $\text{IrO}_2/\text{CeO}_2$ , the conversion of  $^*\text{OH}$  to  $^*\text{O}$  is the RDS. The calculated overpotential of  $\text{IrO}_2/\text{CeO}_2$  is 0.28 V, much smaller than that of  $\text{IrO}_2$  (0.43 V). This trend is highly consistent with the experimental results of the mass activity (Fig. 4c). Incorporation with  $\text{CeO}_2$  modifies the intermediate adsorption energies and thus promotes the RDS to enhance catalytic performance.

To deepen the understanding of the mechanism, the Bader charge differences were calculated, which can be regarded as a descriptor of the oxidation states [52]. As shown in Fig. S24, the oxidation states of the active Ir site on  $\text{IrO}_2$  show significant changes with different adsorption species. However, the oxidation states of the active Ir site on the  $\text{IrO}_2/\text{CeO}_2$  surface are relatively less changed during the catalytic reaction. The  $\text{IrO}_2$  model with  $^*\text{O}$  species shows Ir's most positive oxidation states. In the case of the  $^*\text{O}$  adsorbed on the  $\text{IrO}_2/\text{CeO}_2$  model, most of the Ir-O bonds are longer than those of  $\text{IrO}_2$  (Fig. S25). Bond length between metal and oxygen can influence the oxidation states of metal centers [53]. Herein, the longer Ir-O bonds weaken the interaction between Ir and O and hinder the electron transfer from Ir to O, preventing the active sites from over-oxidized. Besides the Ir-O bond length, the flexible Ce-O bonds are also crucial to regulating the oxidation state of Ir.  $\text{CeO}_2$  with high oxygen mobility can significantly improve the flexibility of the Ir-O bond at the interface of  $\text{IrO}_x$  and  $\text{CeO}_2$  [54]. As shown in Fig. S26, the Ce-O bond lengths show a wide distribution in the range of 2.05–2.90 Å, in which the long Ce-O bonds (> 2.35 Å) are mainly located at the  $\text{CeO}_2/\text{IrO}_2$  interface. These long Ce-O bond lengths show a significant variation with the change of adsorbed species (Fig. S27). The Bader charge difference of Ir shows a strong correlation with the standard deviation of Ce-O bond length, indicating that oxygen species at the interface of  $\text{CeO}_2$  and  $\text{IrO}_2$  can make a massive surface relaxation turning into a disordered state if the local active sites are going to be over-oxidized. Consequently, the more disordered states exhibit a more flexible coordination pattern, which can effectively homogenize the oxidation states of surface species. Overall,  $\text{CeO}_2$  serves as an electron buffer that regulates and controls Ir's oxidation states by surface relaxation during the OER reaction. This electron buffer prevented the Ir species in  $^*\text{O}$  intermediates from being highly oxidative and highly-energetic  $\text{Ir}^{6+}$  state and reduced the energy barrier of OER.

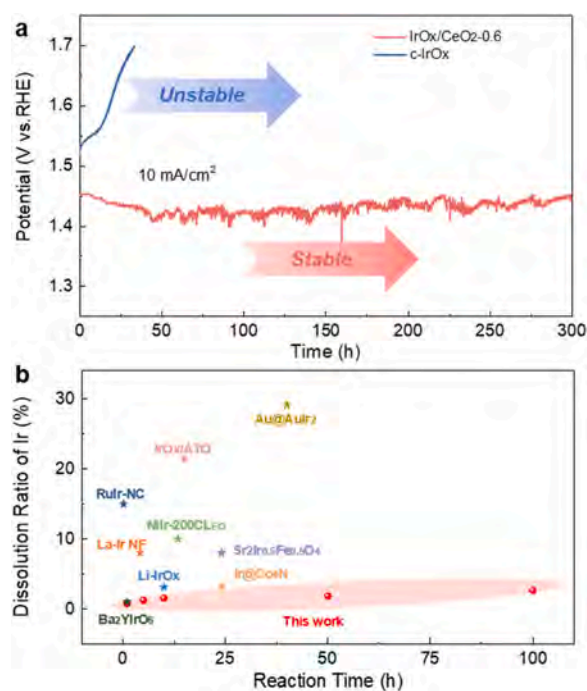
The RDS kinetics and activation energy were verified afterward. To experimentally investigate the participation of H in the RDS, the H/D isotopic experiments were performed by using polarization curves sweeping to explore the roles of the  $\text{CeO}_2$  in the OER process. Fig. S28 shows Tafel plots of  $\text{IrO}_x/\text{CeO}_2-0.6$  and  $\text{c-IrO}_x$  measured in the acidic protium and deuterium solutions. Both catalysts exhibited parallel Tafel curves but slightly inferior OER current in KOD to that in KOH. The  $k_H/k_D$  value was further calculated to be in the range of 2.33–1.79 of  $\text{c-IrO}_x$  and was much higher than that of  $\text{IrO}_x/\text{CeO}_2-0.6$  (1.22–1.25), representing a primary kinetic isotope effect (KIE) that involve H-related bond breaking event in the RDS (Fig. 5c) [55]. Thus, these results indicate that the  $\text{CeO}_2$  play a vital role in facilitating the deprotonation process in the RDS, consistent with the DFT results. We extended the catalytic performance measurements of the  $\text{IrO}_x/\text{CeO}_2-0.6$  and  $\text{c-IrO}_x$

catalysts at various temperatures, and the activation energy ( $E_a$ ) was calculated by plotting the logarithmic values of exchange current density as a function of the inverse of the absolute temperatures (Fig. 5d and Fig. S29). According to the linear relationships,  $E_a$  was determined to be  $28.6 \text{ kJ mol}^{-1}$  for  $\text{IrO}_x/\text{CeO}_2-0.6$  and  $57.4 \text{ kJ mol}^{-1}$  for  $\text{c-IrO}_x$ , respectively [56]. The much lower activation energy of the  $\text{IrO}_x/\text{CeO}_2-0.6$  electrocatalysts suggests their considerably accelerated OER kinetics on the active interfacial sites, in accordance with the superior catalytic kinetics and DFT calculations of the binary amorphous nanowires in acid.

## 2.5. The electron buffer effect for stability

From the perspective of stability, it has been well documented that Ir with a high oxidation state can be easily dissolved into an acidic electrolyte. The electron buffer effect of  $\text{CeO}_2$  suppresses the over-oxidation of the interfacial Ir species. It enables a relatively low oxidation state of Ir, which can greatly improve the stability of  $\text{IrO}_x$  theoretically. As expected, the  $\text{IrO}_x/\text{CeO}_2-0.6$  electrocatalysts indeed delivered an impressively negligible decay of OER performance at  $10 \text{ mA cm}^{-2}$  after a 300 h of continuous operation in  $0.5 \text{ M H}_2\text{SO}_4$  (Fig. 6a). Comparatively, the catalytic activity of  $\text{c-IrO}_x$  was quickly decayed during a period of 30 h, similar to the previous reports. The characterizations of the spent  $\text{IrO}_x/\text{CeO}_2-0.6$  catalysts after stability test, including TEM, HRTEM, EDS, suggested the almost un-alternated structural features in  $\text{IrO}_x/\text{CeO}_2-0.6$ , demonstrating both structural robustness and catalytic stability (Fig. S30).

In order to further confirm the stabilized OER activity of  $\text{IrO}_x/\text{CeO}_2-0.6$  due to the  $\text{CeO}_2$  as the electron buffer and sequentially suppressed Ir dissolution, the inductively coupled plasma mass spectrometry (ICP-MS) measurements were conducted to monitor the electrolyte during chronoamperometric tests. The  $\text{IrO}_x/\text{CeO}_2-0.6$  catalysts exhibited much low Ir dissolution rates of 0.78 %, 1.23 %, 1.56 %, 1.83 %, and 2.64 % of Ir at the time points of 1, 5, 10, 50 and 100 h of continuous operation, respectively, which outperformed the commercially available  $\text{c-IrO}_x$  as well as the majority of the previously reported Ir-based electrocatalysts



**Fig. 6.** OER stability. (a) Chronopotentiometry tests of  $\text{IrO}_x/\text{CeO}_2-0.6$  and  $\text{c-IrO}_x$  at  $10 \text{ mA cm}^{-2}$ . (b) Comparison of the Ir dissolution in this work with the previous literatures.

(Fig. 6b) [21,31,57–63]. Also, ICP-MS results showed that the dissolution of Ir mainly occurred in the early stage and tended to be less in the later stage. The 7.5 % amount of Ce was dissolved after 20 h-stability test, determined from ICP-MS. By examining XPS spectra of Ir before and after stability, the content of trivalent iridium slightly changed from 27.3 % of the initial catalysts to 25.2 % of the spent catalysts (20 h), indicating that the dissolution of Ce might not have a great influence on the surface state of Ir (Fig. S31). The activity of the catalyst was further improved after 20 h-stability test by examining the LSV curves (Fig. S32). By measuring the capacitance of the double layer, it could be concluded that cerium dissolution led to an increase in the electrochemical active area of the catalyst, which could be attributed to the more exposed active sites of Ir species (Fig. S33). Therefore, CeO<sub>2</sub> acts as an electron buffer agent inhibit Ir's dissolution and the electrochemical active area increases, which makes the IrO<sub>x</sub>/CeO<sub>2</sub>-0.6 catalysts highly stable.

### 3. Conclusion

In summary, we have developed a facile, scalable, and cost-effective method to prepare binary amorphous IrO<sub>x</sub>/CeO<sub>2</sub> with nanoscale intimacy as the highly active and durable OER electrocatalysts throughout 300 h of continuous operation in acidic electrolyte. DFT calculations and control experiments demonstrate that CeO<sub>2</sub> serves as an electron buffer to accelerate the kinetics of the rate-determined step for the significantly enhanced activity and suppress the over-oxidation of Ir species as well as their dissolution for impressively promoted stability under practical conditions. Beyond the IrO<sub>x</sub>/CeO<sub>2</sub> electrocatalysts illustrated herein, the strategy of introducing electron buffer can be applied to other acidic OER electrocatalysts, including RuO<sub>x</sub> as well as other Ir-/Ru-compounds.

### CRediT authorship contribution statement

W. Gou and Z. Xia contributed equally to this work. W. Gou carried out the experiments, collected and analyzed the experimental data. Z. Xia helped with the DFT calculations and assisted in the data analysis. X. Tan, Q. Xue, F. Ye, S. Dai, M. Zhang, R. Si, and Y. Zou participated in some of the experimental work. Y. Ma, J. C. Ho, and Y. Qu guided the project and contributed to the result analysis, discussion, and funding acquisition. W. Gou wrote the paper with feedback and guidance from Y. Ma, J. C. Ho, and Y. Qu. All authors discussed the results and commented on the manuscript at all stages.

### Declaration of Competing Interest

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

### Data Availability

Data will be made available on request.

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### Appendix A. Supporting information

Supplementary data associated with this article can be found in the online version at doi:10.1016/j.nanoen.2022.107960.

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